



Stability and Robust Performance Analysis of Fractional Order Controller over Conventional Controller Design

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ABSTRACT

In this paper, a new comparative approach was proposed for reliable controller design. Scientists and engineers are often confronted with the analysis, design, and synthesis of real-life problems. The first step in such studies is the development of a 'mathematical model' which can be considered as a substitute for the real problem. The mathematical model is used here as a plant. Fractional integrals and derivatives have found wide application in the control of dynamical systems when the controlled system and the controller are described by a set of fractional order differential equations. Here the stability and robustness of fractional order system is checked at the different level and it is found that the stability region is large in the complex plane. This large stability region provides the more flexibility for system implementation in the control engineering. Generally, an analytically or experimentally approaches are used for designing the controller. If a fractional order controller design approach used for a given plant then the controlled parameter gives the better result.

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1. INTRODUCTION

The technique model order reduction is used in all fields of electrical, chemical, aerospace, mechanical etc. In the large process control system and mechanical production houses, the model order reduction plays an important role to take the decision for the final product [1-3]. Generally, the work with large scale system is very complex and time-consuming [4]. To check the stability of the system first we make a mathematical model of the plant. If the original system model does not match the desired performance of the implementing system, then a controller is designed to fulfill the requirement of the industry. The designed controller may be a full order or it may be fractional order. The implementation of the controller depends on the plant. If a control system satisfies their stability conditions by the Routh-Hurwitz stability criteria [5] then any analytical or experimental approaches are used. On the other hand, if control system requires the stability region beyond the Routh-Hurwitz criteria or it requires more flexibility [6-9] than

what an approach is useful? So to fulfill the stability condition beyond the Routh- Hurwitz criteria a fractional order approach [10, 11] is used here to design the controller. Here the comparative analysis provides the option to opt a controller design method for the given plant.

2. PID CONTROLLER TRANSFER FUNCTION

The block diagram for a PID controller is shown in Figure 1. The PID controller may be represented in mathematical form as follows:

$$u(t) = k_1[e(t) + \frac{1}{T_i} \int_0^t e(t)dt + T_d \frac{de(t)}{dt}] \quad (1)$$

With the given block diagram $u(s)$ denote control signal and $e(s)$ denotes the error signals of the system. Here k_1 represent the proportion gain and T_i, T_d used for the integral and derivative time constants respectively. The transfer function $G_c(s)$ of the corresponding PID controller is given as

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$$G_c(s) = k_1 \left[1 + \frac{1}{T_i s} + T_d s \right] \tag{2}$$

Equation (2) can be rewritten as

$$G_c(s) = k_1 + \frac{k_2}{s} + k_3 s \tag{3}$$

Here k_2 and k_3 used for integral gain and derivative gain values of the controller respectively.

The objective is to derive a controller such that the performance of the augmented process matches with the desired performance of the model. In the computational system, the desired performance should be satisfied by the closed loop control system [12, 13]. To fulfill these entire requirements a PID controller is derived in form of full order and fractional order.

3. FRACTIONAL ORDER SYSTEM FUNDAMENTALS

3.1. Introduction to Fractional Calculus The term “fractional-order calculus” is not new. It is a generalization of ordinary differentiation by non-integer derivatives. The theory of fractional-order derivatives was mainly developed in 19th century [14-17]. In the development of fractional order calculus, there appeared different definitions of fractional-order differentiation and integration [18, 19]. To reduce to a general form fractional calculus from integration and differentiation to the fractional order fundamental operator ${}^\alpha D_t^\beta f(t)$, where α and t are the limit and $\beta \in R$ is the directive of operation. The continuous integration differential operator is [20]:

$${}^\alpha D_t^\beta f(t) = \begin{cases} \frac{d^\beta}{dt} \dots \beta > 0 \\ 1 \dots \beta = 0 \\ \int_\alpha^t (d\tau)^{-\beta} \dots \beta < 0 \end{cases} \tag{4}$$

There are various definitions for fractional integration and differentiation. Some of the definitions spread out directly as of integer-order calculus. The deep-rooted descriptions include the Cauchy integral formula, the Grunwald–Letnikov (GL) definition and Riemann–Liouville (RL) definitions are given [20] as:

Definition 1: - Cauchy integral formula

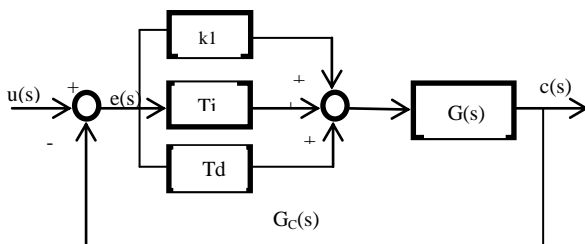


Figure 1. PID controller block diagram

$$D^\gamma f(t) = \frac{\Gamma(\gamma-1)}{2\pi j} \int_c \frac{f(\tau)}{(\tau-t)^{\gamma+1}} d\tau \tag{5}$$

where, c is the smooth curve encircling the single value function $f(t)$

Definition 2: - Grunwald–Letnikov (GL) definition:

$${}^\alpha D_t^\beta f(t) = \lim_{h \rightarrow 0} h^{-\beta} \sum_{j=0}^{\lceil \frac{t-\alpha}{h} \rceil} (-1)^j \binom{\beta}{j} f(t-jh) \tag{6}$$

Here the term in [.] represent the integer part.

Definition 3: - Riemann–Liouville (RL) definition:

$${}^\alpha D_t^\beta f(t) = \frac{1}{\Gamma(n-\beta)} \frac{d^n}{dt^n} \int_\alpha^t \frac{f(\tau)}{(t-\tau)^{\beta-n+1}} d\tau \tag{7}$$

The following function given below is obtained by Laplace Transform of the GL and RL fractional differential-integral. The zero initial conditions and order β gives the following result:

$$\ell[{}^\alpha D_t^\beta f(t); s] = s^{\pm\beta} F(s) \tag{8}$$

3.2. Fractional Order System The fractional-order system is the extension form of the traditional integer order systems. Fractional order system is gained from the fractional-order differential equations. A classic n -term linear fractional order differential equation (FODE) is assumed by:

$$\alpha_n D_t^{\beta_n} y(t) + \dots + \alpha_1 D_t^{\beta_1} y(t) + \alpha_0 y(t) = 0 \tag{9}$$

Let considering the control function on which input signal is applied to FODE system Equation (9) as follows:

$$\alpha_n D_t^{\beta_n} y(t) + \dots + \alpha_1 D_t^{\beta_1} y(t) + \alpha_0 y(t) = u(t) \tag{10}$$

After Laplace transform of Equation (10), we get:

$$\alpha_n s_t^{\beta_n} Y(t) + \dots + \alpha_1 s_t^{\beta_1} Y(t) + \alpha_0 s_t^{\beta_0} Y(t) = U(t) \tag{11}$$

From Equation (11), we can obtain a fractional-order transfer function as

$$G(s) = \frac{Y(s)}{U(s)} = \frac{1}{\alpha_0 s^{\beta_0} + \alpha_1 s^{\beta_1} + \dots + \alpha_n s^{\beta_n}} \tag{12}$$

In broad, for a dynamic system with single variable and fractional order transfer function of a system can be defined as:

$$G(s) = \frac{b_0 s^{\gamma_0} + b_1 s^{\gamma_1} + \dots + b_m s^{\gamma_m}}{a_0 s^{\beta_0} + a_1 s^{\beta_1} + \dots + a_n s^{\beta_n}} \tag{13}$$

Here $b_i (i = 0, 1 \dots m)$, $a_i (i = 0, 1 \dots n)$ are constant and $\gamma_i (i = 0, 1 \dots m)$, $\beta_i (i = 0, 1 \dots n)$ are random real or rational

number and without lacking generality, can be prescribed as $\gamma_m > \gamma_{m-1} > \dots > \gamma_0$ and $\beta_m > \beta_{m-1} > \dots > \beta_0$.

The incommensurable fractional order system Equation (13) can also be expressed incommensurable form by the multi-valued transfer function:

$$H(s) = \frac{b_0 s^{\frac{1}{v}} + b_1 s^{\frac{1}{v}} + \dots + b_m s^{\frac{m}{v}}}{a_0 s + a_1 s^{\frac{1}{v}} + \dots + a_n s^{\frac{n}{v}}}, (v > 1). \tag{14}$$

Note that every fractional order system may be represented in the form of Equation (14) and domain of H(s) meaning is a Riemann sheets.

4. STABILITY OF FRACTIONAL ORDER SYSTEM

Stability is one of the most frequent terms used in literature when we deal with the dynamical systems and their behaviors. In mathematical vocabulary, stability theory addresses the convergence clarifications of differential or difference equations. A system (LTI) is said to be stable if the roots of characteristics polynomial had negative real part. In the case of fractional order system (LTI), the stability is not same as of integer one. Important point is that, for a fractional order system, the roots may lie on the right half of complex plane Figure 2.

Theorem: - According to Matignon's stability theorem the fractional order transfer function $G(s) = \frac{N(s)}{D(s)}$

is stable if and only if $|\arg(\sigma_i)| = q \frac{\pi}{2}$, where $\sigma = s^q$, ($0 < q < 2$) with $\forall \sigma_i \in C$, i^{th} root of $D(\sigma) = 0$.

If $s = 0$, is a single root of D(s), the system cannot be stable.

Above theorem stability region is shown in Figure 2, Indicate the whole s plane where $q = 0$. It shows the Routh-Hurwitz stability and $q = 1$ tends to the negative real axis for $q = 2$.

As we know that only the poles play an important role in the stability of a system. So the stability assessment is done by denominator only and numerator does not affect the stability of an FOTF.

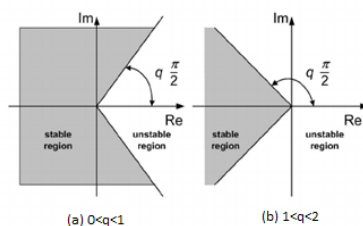


Figure 2. Stable and unstable region of LTI fractional order system

The stability of fractional order system can be analyzed in another way also. Let considering here, the characteristic equation of a general fractional order system as:

$$\alpha_0 s^{\beta_0} + \alpha_1 s^{\beta_1} + \dots + \alpha_n s^{\beta_n} = \sum_{i=0}^n \alpha_i s^{\beta_i} = 0 \tag{15}$$

For $\beta_i = \frac{v_i}{v}$, we can transform the Equation (15) into the σ -plane.

$$\sum_{i=0}^n \alpha_i s^{\frac{v_i}{v}} = \sum_{i=0}^n \alpha_i \sigma^{v_i} = 0 \tag{16}$$

Here $\sigma = s^{\frac{k}{m}}$ and m is the least common multiple of v.

For a given α_i , if the absolute phase of all roots of transform Equation (16) is $|\phi_\sigma| = |\arg(\sigma)|$, we can close the following points for the stability of fractional order systems.

1. The stability condition is as $\frac{\pi}{2m} < |\arg(\sigma)| < \frac{\pi}{m}$.
2. The oscillation condition is as $|\arg(\sigma)| = \frac{\pi}{2m}$.

If any linear time invariant (LTI) fractional order system satisfy the above two points then the system is stable otherwise unstable.

5. FRACTIONAL ORDER CONTROLLER DESIGN

Maximum of the works in fractional order control systems are in hypothetical nature. Controller design and application in run-through is very small. In this paper, the core objective is to spread on the fractional order control (FOC) to examine the system control performance. The fractional-order $PI^\lambda D^\mu$ controller was proposed as a broad view of the PID controller with integrator of real order λ and differentiator of real order μ . The transfer function of such kind the controller in Laplace domain has form:

$$C(s) = K_p + \frac{K_I}{s^\lambda} + K_D s^\mu, (\lambda, \mu > 0) \tag{17}$$

Here K_p is the proportional gain constant K_I is the integral gain constant and K_D is the derivative gain constant. If $\lambda=1$ and $\mu=1$, we obtained a classical PID controller. If $\lambda=0$ and $\mu=0$, we obtained a PD^μ and PI^λ controller respectively. These entire controllers are the case of $PI^\lambda D^\mu$ controller, which provides flexibility with an opportunity to adjust the dynamic property of fractional order control system. Two steps are used here to design such controllers.

Step 1: - Design of K_p

Overshoot in percentage [Pr], settling time in second [Ts] and static error in percentage [Et] belongs to Proportional gain K_p . In general, K_p can be obtained by:

$$K_p \geq \left(\frac{100}{E_t} \right) \tag{18}$$

Here Proportional gain K_p is selected for minimum static error.

Step 2: - Design of K_D, μ, K_I and λ

To determine these values for Fractional-Order controller design, the following synthesis scheme is used here.

Let the controller transfer function is $C(s)$, plant transfer function is $G(s)$ and a unity feedback is applied to the system. Phase margin of controlled system [21, 22] is:

$$\Phi_m = \arg[C(j\omega_g)G(j\omega_g)] + \pi \tag{19}$$

Here $j\omega_g$ is the crossover frequency. Phase margin is an independent or constant phase. This can be accomplished by controller of the form:

$$C(s) = k_1 \frac{k_2 s + 1}{s^\nu}, k_1 = \frac{1}{K_{plant}}, k_2 = \tau \tag{20}$$

Here K_{plant} is the gain of plant and τ is the time constant for the plant.

Now from Equations (19) and (20)

$$\left\{ \begin{aligned} \phi_m &= \arg[C(j\omega_g)G(j\omega_g)] + \pi \\ &= \arg\left[\frac{k_1 k_{plant}}{j\omega^{(1+\nu)}}\right] + \pi \\ &= \arg[(j\omega)^{-(1+\nu)}] + \pi \\ &= \pi - (1+\nu)\frac{\pi}{2} \end{aligned} \right. \tag{21}$$

Here for a given plant, we fix the gain margin. Put the gain value in Equation (21) one can find out the value of ν . the other desired values k_1 and k_2 are obtained from Equation (20).

Now using these constant in Equation (20), we can obtain a fractional $I^{\lambda}D^{\mu}$ controller, which is a particular case of $PI^{\lambda}D^{\mu}$ controller has the form

$$C(s) = k_1 k_2 s^{(1-\nu)} + k_1 s^{-\nu}; K_D = k_1 k_2 \text{ and } K_I = k_1 \tag{22}$$

If the value of K_p is given then the full transfer function of fractional order controller is

$$C(s) = K_p + K_D s^{(1-\nu)} + K_I s^{-\nu} \tag{23}$$

If do a comparison with Equation(17), we can say $\mu = (1-\nu)$ and $\lambda = \nu$.

6. CONTROLLER DESIGN USING ZIEGLER-NICHOLS SECOND METHOD

In this method, we first set $T_i = \infty$ and $T_d = 0$. By using the proportional control action increase K from 0 to a critical value K_{cr} at which the output exhibits sustained oscillations in the system.

Thus, the critical gain K_c and the corresponding period P_{cr} are determined by experiment. According to Ziegler-Nichols method the values of the parameters K_p, T_i and T_d can be obtained by the formulas shown in Table 1.

The PID controllers tuned by the second method of Ziegler-Nichols rules give [15].

$$G_c(s) = K_p \left(1 + \frac{1}{T_i s} + T_d s \right) = 0.6 K_{cr} \left(1 + \frac{1}{0.5 P_{cr} s} + 0.125 P_{cr} s \right) \tag{24}$$

$$= 0.075 K_{cr} P_{cr} \frac{\left(s + \frac{4}{P_{cr}} \right)^2}{s} \tag{25}$$

Equation (25) shows that the PID controller has a pole at the origin and double zeros at $s = -\frac{4}{P_{cr}}$.

7. SENSITIVITY AND ROBUSTNESS ANALYSIS

If the controller and plant transfer function is $C(s)$ and $P(s)$ respectively then the sensitivity function may be defined as:

$$\frac{1}{1 + PC} \tag{26}$$

Let the disturbance is subjected to open loop and closed loop system as shown in Figure 4.

Tracking the signal for the loop shown in Figure 4, the exponential signal with output is

$$y_{cl}(t) = \frac{1}{1 + P(s)C(s)} S(s) y_{ol}(t) \tag{27}$$

where, $S(s)$ is the sensitivity function.

To follow references closely and to reject the output disturbances, the sensitivity function must have a small magnitude at low frequencies; hence, its magnitude is to be less than some specified gain L [23] at some specified frequency ω_1 .

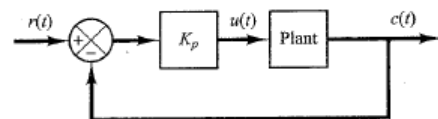


Figure 3. Closed loop system for proportional controller

TABLE 1. For critical gain and critical period

Type of controller	K_p	T_i	T_d
P	$0.5 K_{cr}$	∞	0
PI	$0.45 K_{cr}$	$1/1.2 P_{cr}$	0
PID	$0.6 K_{cr}$	$0.5 P_{cr}$	$0.125 P_{cr}$

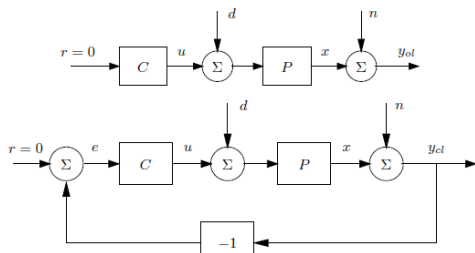


Figure 4. Open and closed loop systems subject to the same disturbances

$$\left| \frac{1}{1 + C(j\omega_1)P(j\omega_1)} \right| < L \tag{28}$$

The robustness of the system occurs if the gain variation exists in the system and at the gain-crossover frequency the phase of the open-loop transfer function is to be (at least roughly) constant.

$$\frac{d}{d\omega} \arg[C(j\omega)P(j\omega)] \Big|_{\omega=\omega_{cg}} = 0 \tag{29}$$

8. EXAMPLES

Here we are conceding the general model [24] of DC motor as shown in Figure 5. The angular velocity $\omega(t)$ is controlled by the applied voltage V_a .

The mathematically model of the DC Motor is given as in Figure 6. The obtained transfer function of the DC Motor is

$$G_{DCM}(s) = \frac{\theta(s)}{V_a(s)} = \frac{K_m}{s[(Ls + R)(Js + K_f) + K_b K_m]} \tag{30}$$

In most application the time constant of DC Motor is negligible therefore the simplified continuous mathematical model has the following form:

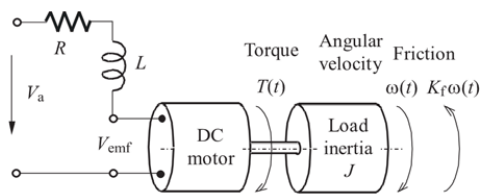


Figure 5. General model of DC Motor

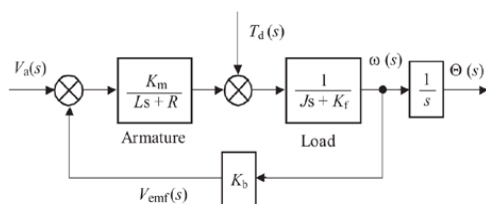


Figure 6. Mathematical model of a DC Motor

$$G_{DCM}(s) = \frac{\theta(s)}{V_a(s)} = \frac{K_m}{s[R(Js + K_f) + K_b K_m]} \tag{31}$$

$$= \frac{K_{DCM}}{\tau(s + 1)}$$

where, $\tau = \frac{RJ}{(RK_f + K_b K_m)}$ and $K_{DCM} = \frac{K_m}{(RK_f + K_b K_m)}$. It is also note that $K_m = K_b$

For the give DC Motor the physical parameter are as

- $R = 6\Omega$
- $K_m = K_b = 0.1$
- $K_f = 0.2N - ms$
- $J = 0.01kgm^2 / s^2$

With the help of given constant, obtained transfer function is

$$G_{DCM}(s) = \frac{0.08}{s(0.05s + 1)} \tag{32}$$

8.1. Controller Design by Ziegler-Nichols Method with Stability and Sensitivity Analysis

The first requirement is to find out the starting point for K_p and double zeros.

Let start the tuning with considering the K_p only.

Here the closed loop response is:

$$G_{clZN} = \frac{C(s)}{R(s)} = \frac{0.08K_p}{s(0.05s + 1) + K_p} \tag{33}$$

By the help of Routh-Hurwitz criteria, the value of K_p for sustained oscillations is $K_p \geq 62.5$

We set the value in MATLAB program with a hit and trial range. After putting the values in $G_{clZN}(s) = K_p(1 + \frac{1}{T_i s} + T_d s)$, we find out the controller

transfer function $G_{CZN}(s) = \frac{37.4s^2 + 523.6s + 1833}{s}$

Therefore, here the initial values are obtained. As the requirement of industry, we can set the value of maximum overshoot in programming. Generally, according to the better establishment of the system, the overshoot should be between 10% to 40%. Using the MATLAB program, we vary the gain 120 to 30 with step size -0.2 and zeros as 7 to 0.3 with step size -0.2. Fine tuning gives the following results

Gain (K) = 37.4 and Zeros (a) = 7

Maximum overshoot (m) = 1.05

The final close-loop transfer function of the system is:

$$G_{clZN}(s) = \frac{2.992s^2 + 41.89s + 146.6}{0.05s^3 + 3.992s^2 + 41.89s + 146.6} \tag{34}$$

The transfer function of open loop and closed loop system with sensitivity from Equation (27) is:

$$G_{sol}(s) = \frac{2.992s^2 + 41.89s + 146.6}{0.05s^3 + s^2} \tag{35}$$

$$G_{scl}(s) = \frac{0.1496s^5 + 5.086s^4 + 49.22s^3 + 146.6s^2}{0.0025s^6 + 0.3992s^5 + 11.17s^4 + 98.44s^3 + 293.3s^2} \tag{36}$$

Figure 7 shows the stability region and Figure 8 Shows the step response of the system. The Bode plot of open loop and closed loop system is shown in Figure 9. Here the designed controller is by Ziegler-Nichols Method. The specification of gain crossover frequency and phase margin are obtained. The phase of the given system is forced to be flat at ω_{cg} and hence to be almost constant within an interval around ω_{cg} .

8. 2. Stability Check and Robust Controller Design by Fractional-Order Method A robust controller is less sensitive to the parameter changes of the controlled system [25]. The uncertainty can be caused by non-precise identification. The fractional order controllers are less sensitive to changes of controlled system parameters.

The FOPDT system with parametric uncertainty can be represented as:

$$G(s) = \frac{[k, \bar{k}]}{s([\tau, \bar{\tau}]s + 1)} \tag{37}$$

where, \bar{k} , $\bar{\tau}$ and \underline{k} , $\underline{\tau}$ are the upper and lower limits of the given parameters.

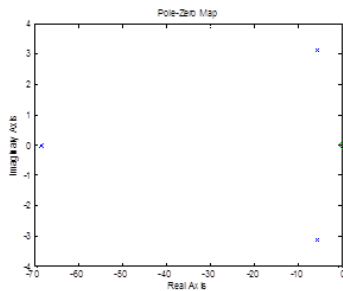


Figure 7. Pole location on Pole-Zero Map of GclZN(s)

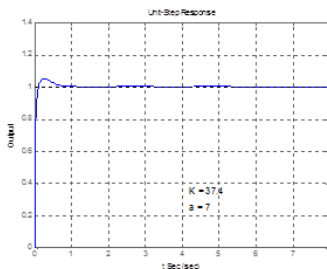


Figure 8. Unit step response of the closed loop GclZN(s) system

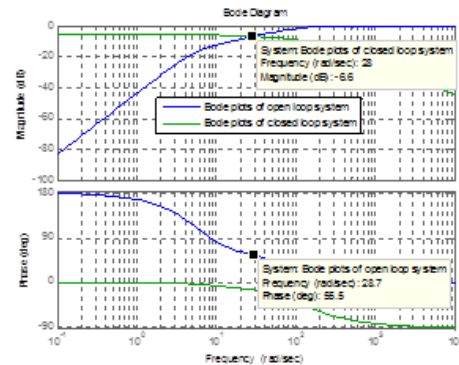


Figure 9. Bode plots of open loop Gsol(s) and closed loop Gscl(s) system

For maximum and minimum gain plot, the given system transfer function are shown respectively as:

$$G_{R1}(s) = \frac{[k]}{s([\tau]s + 1)} \tag{38}$$

$$G_{R2}(s) = \frac{[\bar{k}]}{s([\bar{\tau}]s + 1)} \tag{39}$$

Consider the transfer function model of plant in given example is:

$$G_{Plant} = \frac{0.08}{s(0.05s + 1)} \tag{40}$$

We are using here the technique proposed in section 4 for fraction order controller design. According to this Step 1: - To design the K_p

For minimum static error the value of proportional gain K_p=10, from Equation (40)

Step 2: - Design of K_D, μ, K_I and λ

The value of a time constant τ = 0.05 and gain of Plant K_{Plant} = 0.08 respectively Equation (40).

If we fix to gain margin φ_m ≥ 60° for the given control system. Then we find out the value of v = 0.3 by Equation(21). The other desired value k₁ = 12.5 and k₂ = 0.05 obtained from Equation (20). Now putting these values in Equation (22), we got

$$C_{FO}(s) = 0.625s^{0.7} + \frac{12.5}{s^{0.3}} \tag{41}$$

Now add the value of K_p = 10 from step 1 into Equation (41), we got final transfer function of fractional order controller as:

$$C_{FO}(s) = 10 + 0.625s^{0.7} + \frac{12.5}{s^{0.3}} \tag{42}$$

To make robust of the system an obtained controller transfer function is used with the transfer function

obtained for maximum and minimum gain as given in Equations (38) and (39). The open loop control system for controller and plant $G_{R1}(s)$ is:

$$G_{R1_{ol}}(s) = \frac{0.0625s + s^{0.3} + 1.25}{0.04s^{2.3} + s^{1.3}} \quad (43)$$

The close-loop transfer function of given control system with unity feedback is obtained as:

$$G_{R1_{cl}}(s) = \frac{C(s)G_{Plant}(s)}{1 + C(s)G_{Plant}(s)}$$

or

$$G_{R1_{cl}}(s) = \frac{0.0625s + s^{0.3} + 1.25}{0.04s^{2.3} + s^{1.3} + 0.0625s + s^{0.3} + 1.25} \quad (44)$$

The open loop control system for controller and plant $G_{R2}(s)$ is:

$$G_{R2_{ol}}(s) = \frac{0.6s + 0.03750s^{0.3} + 0.750}{0.06s^{2.3} + s^{1.3}} \quad (45)$$

The close-loop transfer function of given control system with unity feedback is obtained as:

$$G_{R2_{cl}}(s) = \frac{0.3750s + 0.6s^{0.3} + 0.750}{0.06s^{2.3} + s^{1.3} + 0.03750s + 0.6s^{0.3} + 0.750} \quad (46)$$

The function is *stable* checked the denominator of $G_{R1_{cl}}(s)$ and $G_{R2_{cl}}(s)$, it is found that $K=1$, indicate the system is stable. Here Figures 10 and 11 shows that system controlled by fractional order controller has more stability region. Figure 12 Indicate that the complete designed system is stable. The closed loop response of the system for both plants is almost same. This means that due to the parameter variation there is no such effect on the stability and system has a robust performance as shown in Figure 13.

9. CONCLUSIONS

On behalf of the result shown in Table 2, some important point may be described for tuning of the controller.

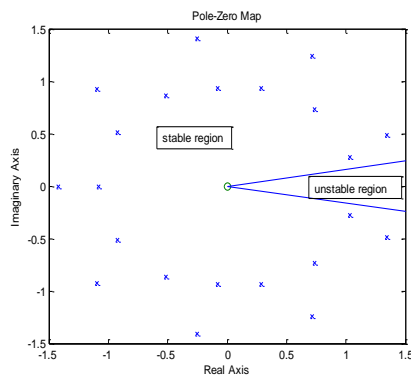


Figure 10. Pole position of a closed loop system $G_{R1_{cl}}(s)$

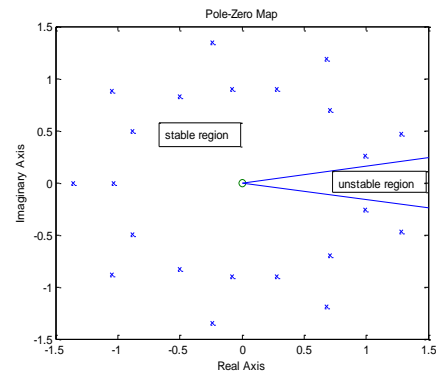


Figure 11. Pole position of a closed loop system $G_{R2_{cl}}(s)$

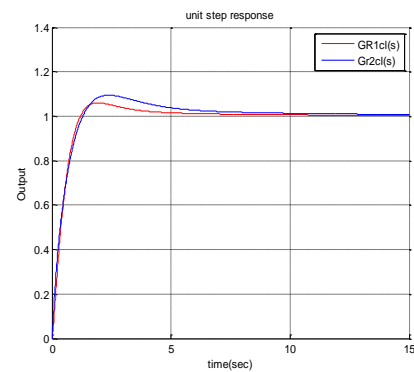


Figure 12. Step response of closed loop system $G_{R1_{cl}}(s)$ and $G_{R2_{cl}}(s)$

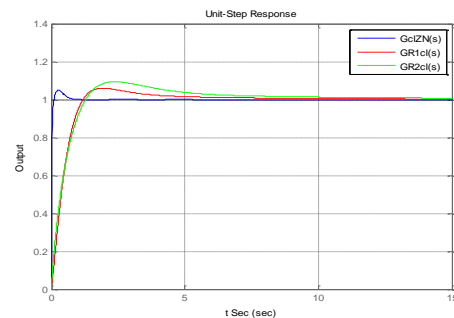


Figure 13. Simultaneously unit step response of all designed systems

All basic ideas of fractional calculus, the stability of fractional order system, sensitivity, robustness and MATLAB function are presented here. The robustness and sensitivity analysis is investigated for the given real-time example. The main purpose of the paper is to draw attention to fractional order system stability and analysis over a conventional way. Here an integer order plant is controlled by full order controller and fractional order controller. It concludes here that the fractional order system has robustness and a large region for

stability which improves the performance of the system. In Table 2 all transient parameter of fractional order controller design system and conventional controller design are given. The conventional controller design has a better transient response over fractional order controller design system. But in the fractional order, the larger stability region provides more flexibility in the system. We believe that the comparative approach used in this paper is useful for selecting the method of controller design.

TABLE 2. Comparison for performance specification of designed controllers

Controller design	Ziegler-Nichols Method	Fractional-Order Method	Fractional-Order Method
Models	Full Model	Full Model	Full Model
Specifications	Gc _i ZN (s)	GR1cl (s)	GR2cl(s)
Rise time (s)	0.0454	0.878	0.881
Settling time (s)	0.55	13.2	14
Peak amplitude	1.05	1.06	1.09
Overshoot (%)	5	6	9
At time (s)	0.26	1.87	2.32

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Stability and Robust Performance Analysis of Fractional Order Controller over Conventional Controller Design

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در این مقاله روش مقایسه ای طراحی کنترلر پیشنهاد شده است. دانشمندان و مهندسين با انالیز و طراحی مواردی از مشکلات واقعی مواجه می شوند که در اولین گام تکامل و پیدایش مدل های ریاضی برای حل مشکلات واقعی مورد توجه قرار می گیرد. مدل های ریاضی همانند یک طرح و برنامه قابل اجراست. انتگرال تابع و مشتقات تابع کاربری وسیعی در کنترل سیستمهای دینامیکی دارد. موارد کنترل توسط معادلات دیفرانسیل درجات بالا یا مشتقات جز را در بر می گیرد. در این مرحله پایداری و درجه سیستم مورد بررسی قرار می گیرد. ناحیه پایداری در محدوده و صفحه پیچیده ای قرار می گیرد. ناحیه پایداری وسیع در یکارگیری کنترل مهندسی به سیستم انعطاف پذیری می دهد. بطور کلی طروق حل انالیز عددی و روش تحلیل تجربی بکار گرفته می شود. اگر از روش طراحی کنترل و درجه کنترل اجزا بکار گرفته شود سپس کنترل پارامترها نتایج بهتری می دهد.

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